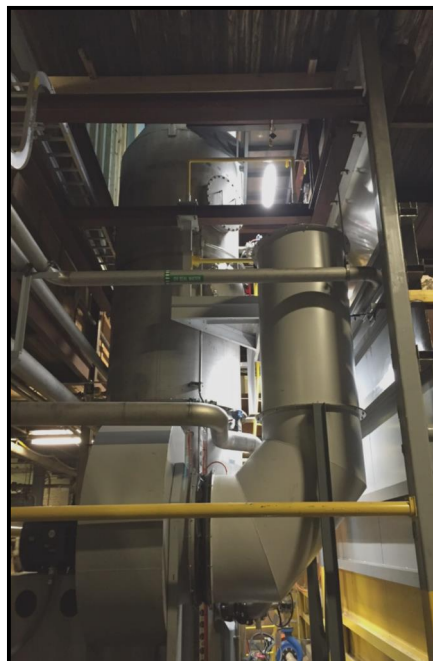


# TurbEx™ FLUID BED-COOLING TOWERS

## CASE STUDY: Huhtamaki Pulp & Paper, U.S.A.

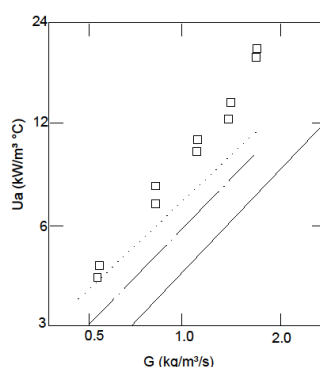
SYSTEM DESIGN DETAILS	
<b>HEAT TRANSFER</b>	
Inlet Water Temp °F	53.3°C
Liquid Medium	White Water
Inlet Air Temp °F	27.8°C
Inlet Approach ΔT °F	< 1.67°C (<3 °F)
Inlet % Approach	99.9%
Design Heat Transfer	7.6 MMBtu/hr (2.2 MW)
Heat Trans Coefficient	See HTC below
<b>FLUID DYNAMICS</b>	
Liquid Flowrate	105m <sup>3</sup> /hr
Operating Mode	Once through
Pressure Drop	6.5" WG (1600 Pa)
<b>TOWER</b>	
Column Diameter	1.83m (6 ft)
Overall Tower Height	7.25 m
Construction Materials	SS 316

Commissioned in late Spring 2016 this **TurbEx™** COOLING TOWER cools process water at a Huhtamaki U.S. pulp & paper facility using TurboScrubber® fluidized packing to ensure continuous non-clogging operation even with sticky pulp & solids laden white water. The system is integrated with the plant process control system to maintain optimum operation.



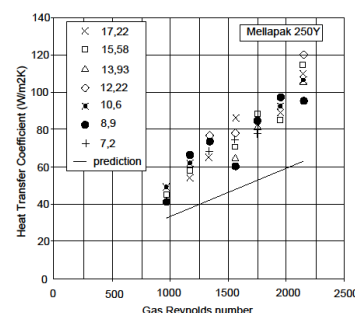
Despite operating during non optimal start up conditions with low water flow, low enthalpy (water inlet 47°C) & high inlet air RH the heat transfer was still at 3.5MMBtu/hr (~1MW) & the outlet water temp within 3°F of the inlet dry bulb gas temp. This equates to a 280 KW/m<sup>3</sup>K expanded bed HTC.

By comparison typical wet gas HTCs shown here for Ceramic Intalox Saddles (left) & Mellapak 250Y structured packing (with its 250m<sup>-1</sup> interface) are reported at between 5 & 30KW/m<sup>3</sup>K.

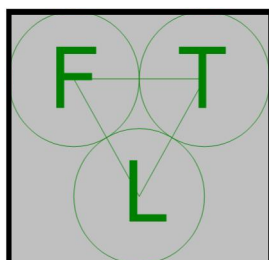


Comparison of Present Model with Results of Huang, L=2.71kg/m<sup>2</sup>

- Huang Data
- Huang Model for  $h_{aig}$
- - - Present Model for  $h_{aig}$
- ..... Present Model for  $U_a$ , 1-1/2" Ceramic Intalox Saddles



Heat transfer coefficient vs Re of middle section of the column (P= 1.5 bar abs)



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